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Model Predictive Control for Flotation Plants



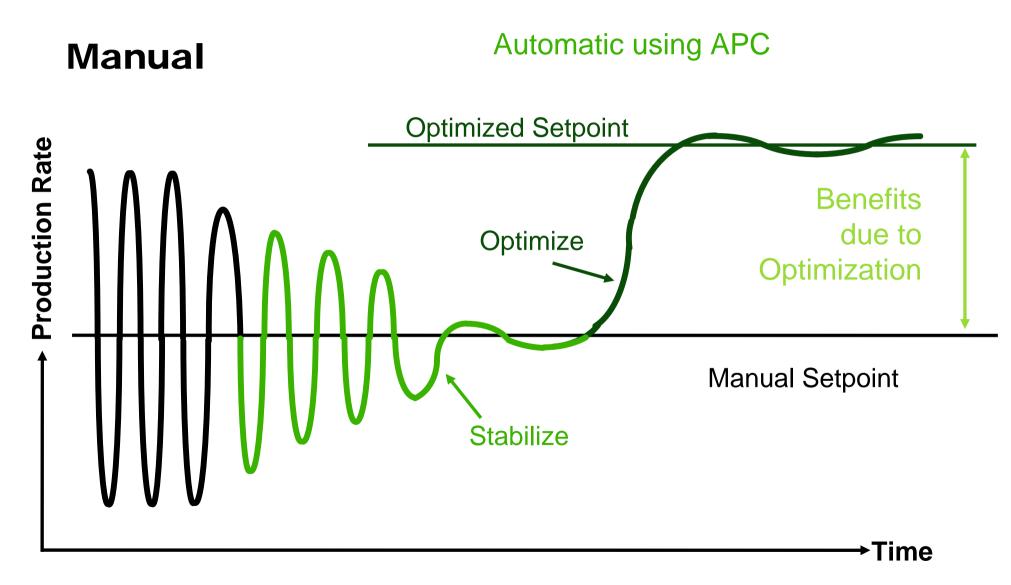
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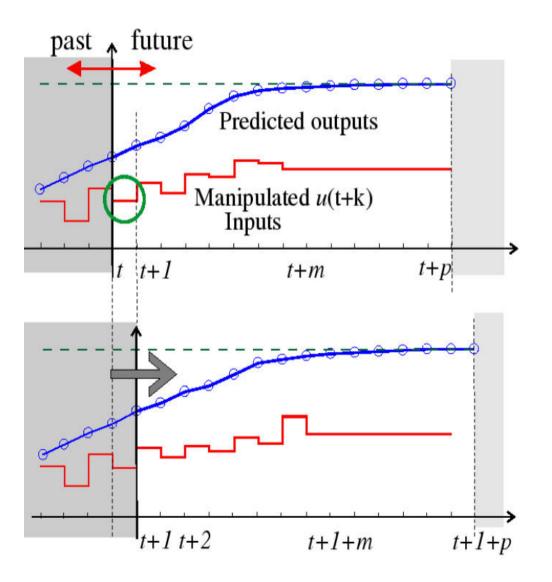


Stabilize then optimize





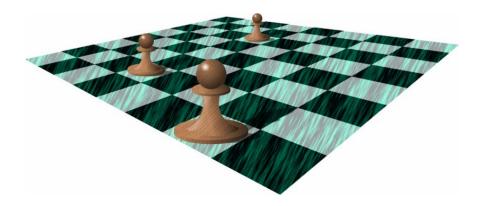
Model Predictive Control (MPC)

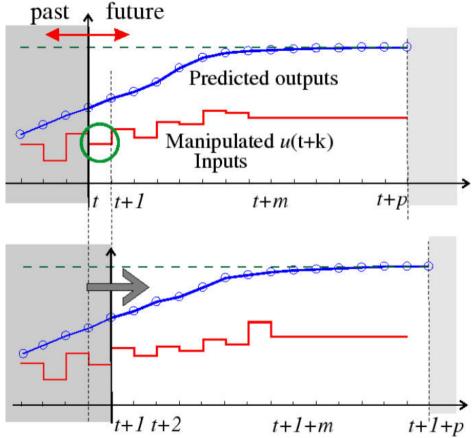


- Main ingredients are
 - Plant model
 - Objective Function
- Model used to predict system behaviour some steps into the future
- Cost Function used to decide which is the best strategy
- Requires solution of optimization problem at every sampling time
- Cost function is normally a sum of of linear and quadratic terms so as to guarantee convexity

Model Predictive Control (MPC)

- Evaluate position (=measurement) and estimate system state
- 2. Predict sequence of future moves (mathematical algorithm, optimization) and select the best
- 3. Implement the first move (new actuator setpoint)
- 4. Restart after the opponent moves (process reaction)





- Constraints are considered (allowed moves)
- A cost function drives the decision process (e.g. improve quality of the position)



Modelling for Model Predictive Control First Principles and/or Black Box Models

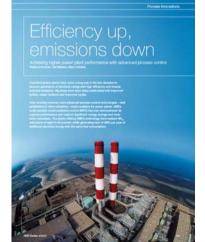
- Models are not necessarily high fidelity models
 - Comprise only magnitudes relevant for the control tasks
 - Often contain information related to gains, time constants, and time delays
 - Must predict only relevant time horizon as given by process time constants
- Two modelling paradigms
 - "First principle models": attempt to describe the relationships via equations based on process knowledge. Selected parameters are adapted online
 - Black Box models: models are generated by looking at plant data. Variables must undergo "excitation" for algorithms to work successfully



Expert Optimizer: ABB's advanced process control platform



- Successor of "Linkman" (Fuzzy Logic), but enhanced with Neural Networks and MPC technology
- DCS independent
- More than 300 installations worldwide
- Global Fuels Conference Award for "most innovative technology for electrical energy savings"



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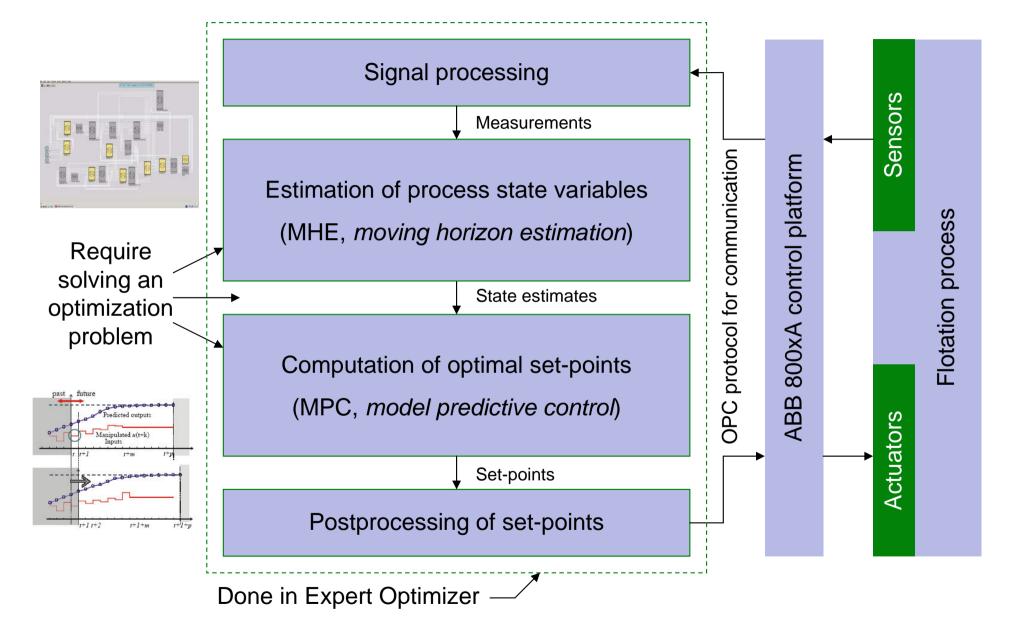
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Tapping technology Control The water back the set of the set



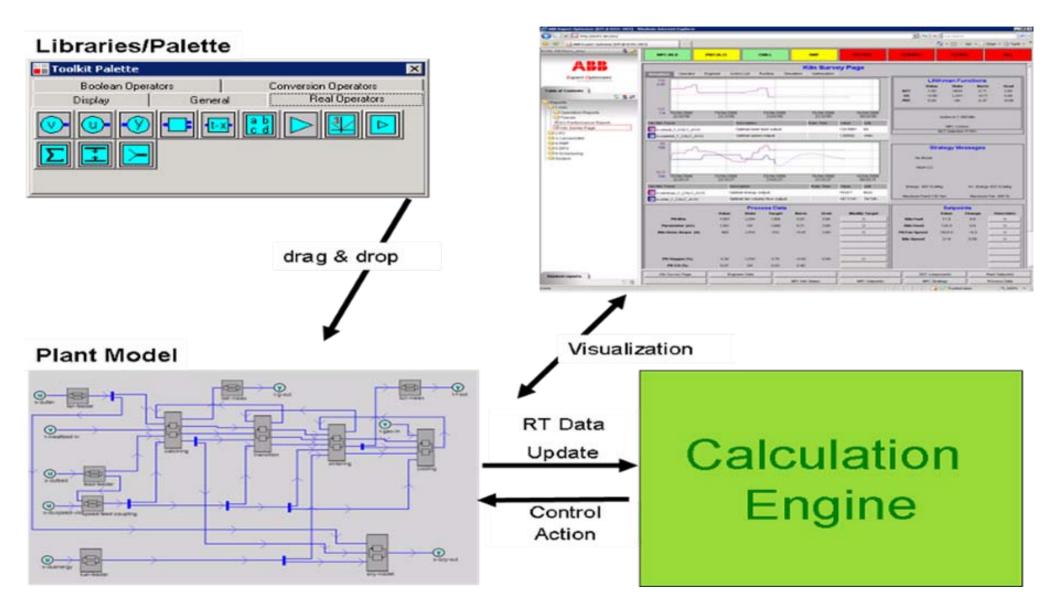


Implementation in Expert Optimizer





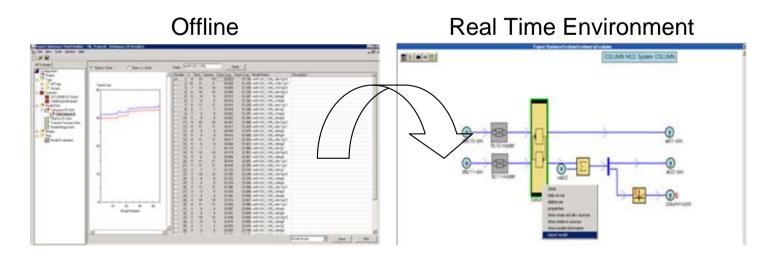
Expert Optimizer – Advanced Process Control Platform





Model Predictive Control in Expert Optimizer First Principles and/or Black Box Models

- Supports both modelling approaches
 - Model building by connecting blocks from a standard library or importing custom made ones
 - Cost function also designed in this form
 - Nonlinear models also supported
- Infrastructure for Black Box identification
 - Environment for handling data import and data set manipulation
 - Subspace identification for model generation
 - Model export with subsequent import in runtime environment





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Flotation: where are we and where do we want to go?

State of the art

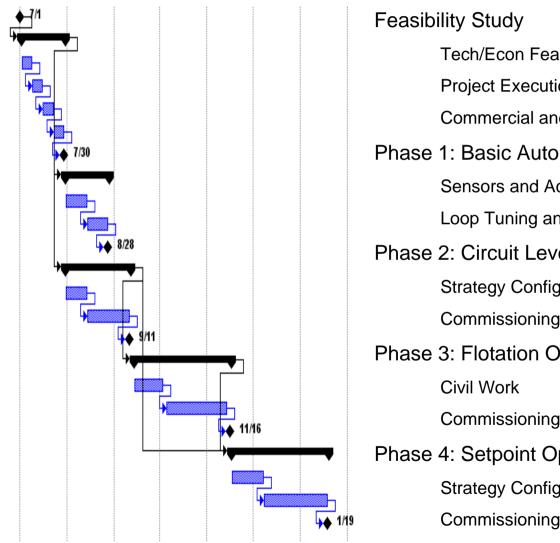
- Manual control, intricate due to
 - dynamics (e.g. recirculating flows),
 - frequent feed variations (quantity and quality), and
 - operator shift changes
- No circuit-wide automatic control widely established

Objectives

- Maximization of plant output
- Observance of minimum concentrate grade
- Reduction of chemical reagent use
- Prevention of costly unplanned plant stops by respecting operating range of plant



Beneficiation Plant Project Phases



| Feasibility Study | | | | | | |
|----------------------------------|--|--|--|--|--|--|
| Tech/Econ Feasibility Analysis | | | | | | |
| Project Execution Plan | | | | | | |
| Commercial and Technical Offer | | | | | | |
| Phase 1: Basic Automation Level | | | | | | |
| Sensors and Actuators Assessment | | | | | | |
| Loop Tuning and Monitoring | | | | | | |
| Phase 2: Circuit Level Control | | | | | | |
| Strategy Configuration | | | | | | |
| Commissioning | | | | | | |
| Phase 3: Flotation Optimization | | | | | | |
| Civil Work | | | | | | |
| Commissioning | | | | | | |
| Phase 4: Setpoint Optimization | | | | | | |
| Strategy Configuration | | | | | | |
| Commissioning | | | | | | |



Expert Optimizer for Circuit Level Control



Objectives

Better control of the cell levels in the entire circuit

Technology

Adjusting the valves between cells, using measurements of the cells levels

Multivariable control problem, solved using MPC technology

Model considers coupling between cells and the effect of actions with the valves on the entire circuit

Benefits

- More production
- Better process stability
- Quality as specified



Expert Optimizer for Flotation Circuit Control



- Objectives
 - Highest possible feed rate
 - Guarantee product quality spec.
 - Increase recovery
 - Reduce reagent usage
 - Prevent froth collapse or overfrothing
- Techniques
 - Model Predictive Control
 - Models
 - Froth Model
 - Slurry Model
 - Coupling between Cells
- Manipulated Variables
 - Reagents, Air Supply, Froth Depth
 - Cell Froth/Slurry Levels!



Next Step: Economic Process Optimization

$$J = Q_C \cdot F(x_C, x_C^{Fe})$$

- What have we achieved so far?
 - MPC controls concentrate and tailings to desired set-points.
 - However, not obvious which set-points to use.
- Method to find best set-points to maximize the value of the production.
 - Assume it is possible to control the flotation process to desired set-points
 - The value of the production depends on the amount of produced mineral, the purity of it, and its market price.
 - Static model of the flotation process as constraint for the optimization

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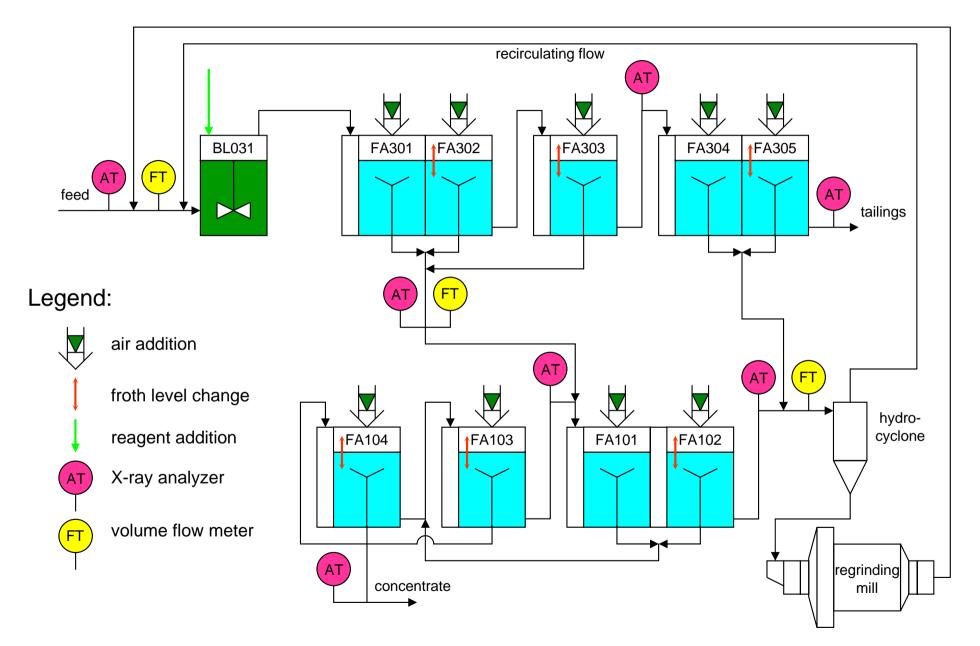
Customer Case: cpmPlus Expert Optimizer in Flotation



- Customer Boliden, Sweden
 - Optimisation of Floatation Cells in Zn
 - Aim Achieve better recovery at given grade
- Approach
 - a) Model using historical data
 - b) Model derived from first principles
- Manipulated Variables
 - Cell level control
 - Air Supply
 - Froth Level
 - Reagents

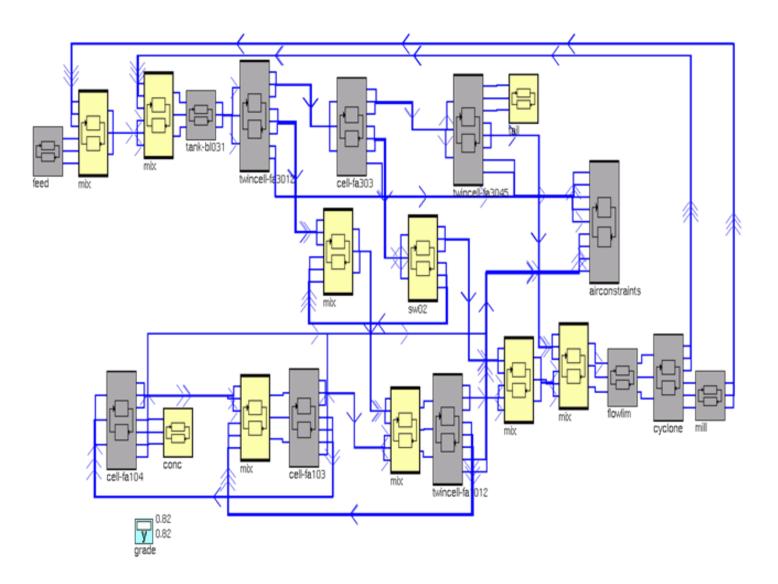


Manipulated and measured variables of a circuit



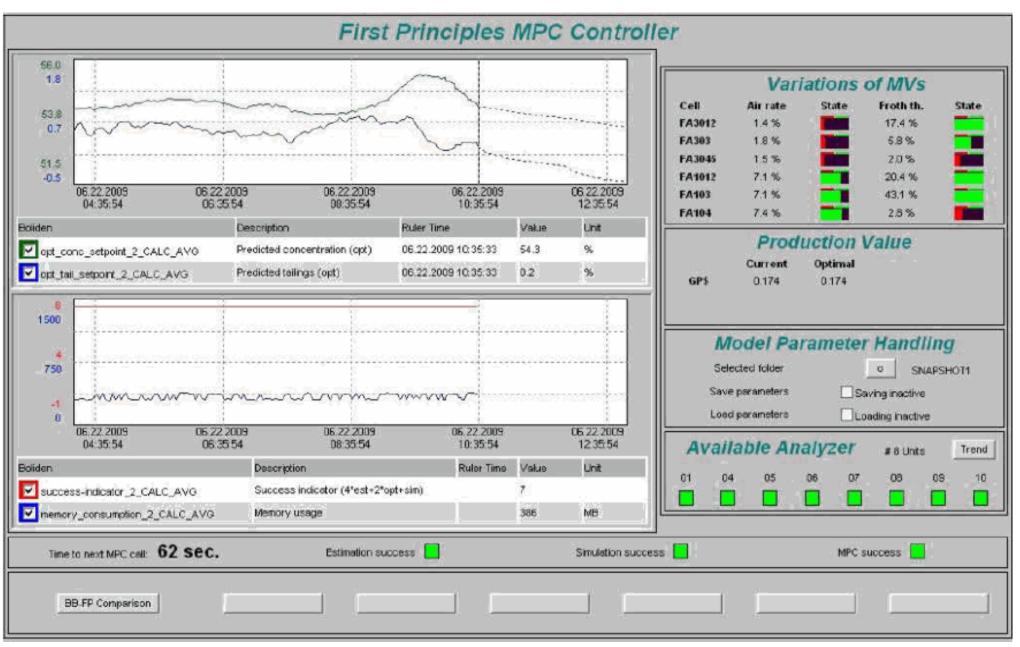


Controller Configuration in Expert Optimizer



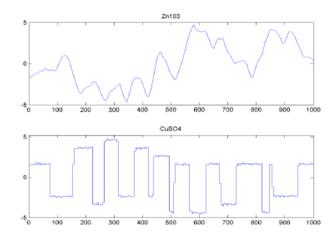


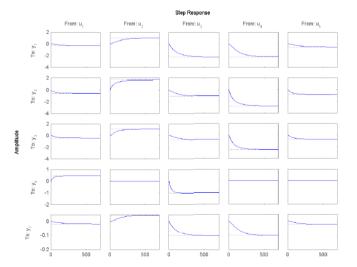
Thin Client User Interface in cpmPlus Expert Optimizer





Grey/Black Box Modeling approach



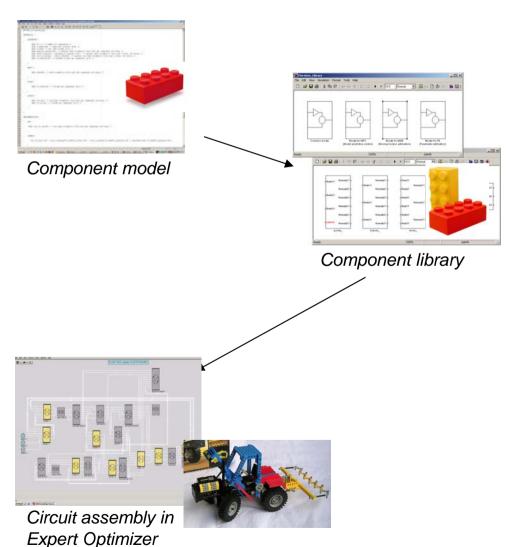


- Experimental phase:
 - What is done:
 - Plant actuators are moved in controlled manner
 - Reaction of process is recorded
 - Objective
 - Excite relevant process variables so that process dynamic becomes visible
 - Constraints
 - Plant conditions, cost and safety
- Modeling phase:
 - Selection of appropriate slices of data
 - Model generation
 - Delicate iterative process

Linearised first-principle approach

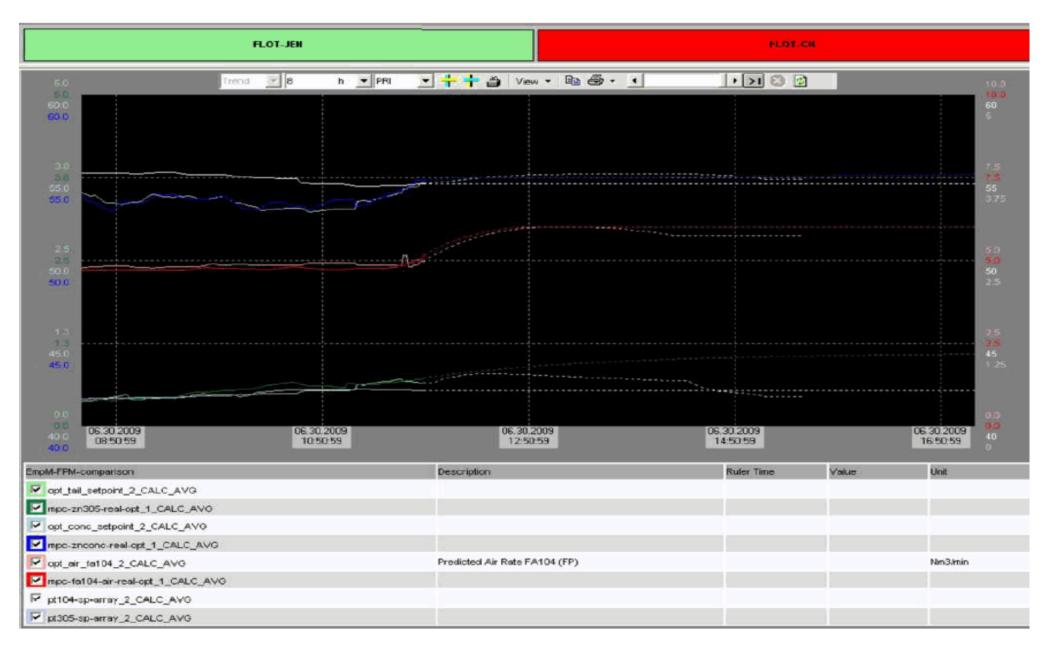
The process model is

- Mechanistic ("first principles")
 - Mass and volume balances
 - Pulp-to-froth transfer model
 - Variables: volumes and volume flows of relevant fractions
- Linearized about an operating point
- Generic and modular (componentwise):
 - flotation cell, mixing tank, ...
 - analyzers, volume flow meters,
 ...
- \rightarrow Objectives:
 - \rightarrow maintainability, reuse





Black Box versus First Principles





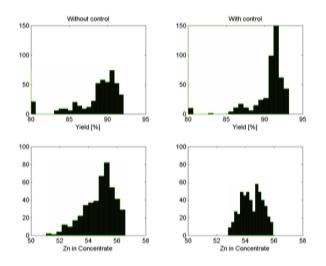
Steady State Model for Setpoint Optimization

$$J = Q_C \cdot F(x_C, x_C^{Fe})$$

- Value of the production depends on the amount of produced mineral, the purity of it, and its market price.
- Value function reflects the plant management objectives
- Static model of the flotation process as constraint for the optimization



cpmPlus Expert Optimizer delivers higher yields



| | Input Zinc | | Concentrate | Tailings | Yield | AE for Zn |
|------------|------------|------|-------------|----------|-------|-----------|
| | ton | % | % | % | % | % |
| On total | 98385 | 7.17 | 53.57 | 0.55 | 90.61 | 88.34 |
| Off total | 121676 | 7.89 | 53.77 | 0.66 | 89.40 | 87.32 |
| On 1 day | 71000 | 7.66 | 53.53 | 0.5 | 90.60 | 8.28 |
| Off 1 day | 82826 | 8.07 | 53.58 | 0.7 | 88.74 | 6.52 |
| On 2 days | 22465 | 6.66 | 54.36 | 0.50 | 91.43 | 89.78 |
| Off 2 days | 27380 | 7.40 | 54.81 | 0.57 | 90.08 | 88.80 |

- Black Box approach currently more successful
- Several months on-line testing and comparison with existing manual strategy
 - One to two days on, then one to two days off, etc.
- Value
 - 1% Higher Yield
 - More consistent Zn concentrate
 - Improvement is at least one percentage unit
 - Millions worth

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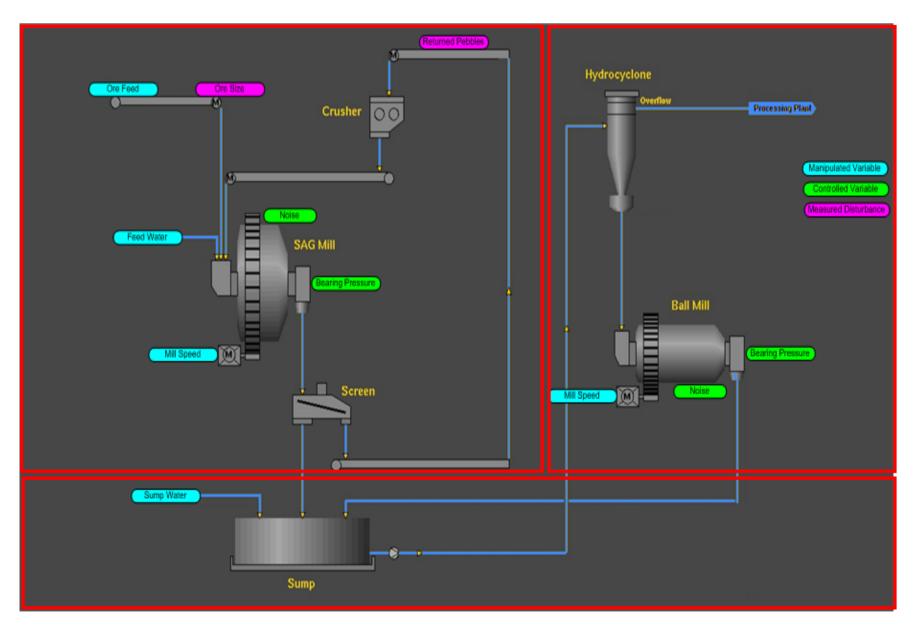
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Grinding Circuit Optimization



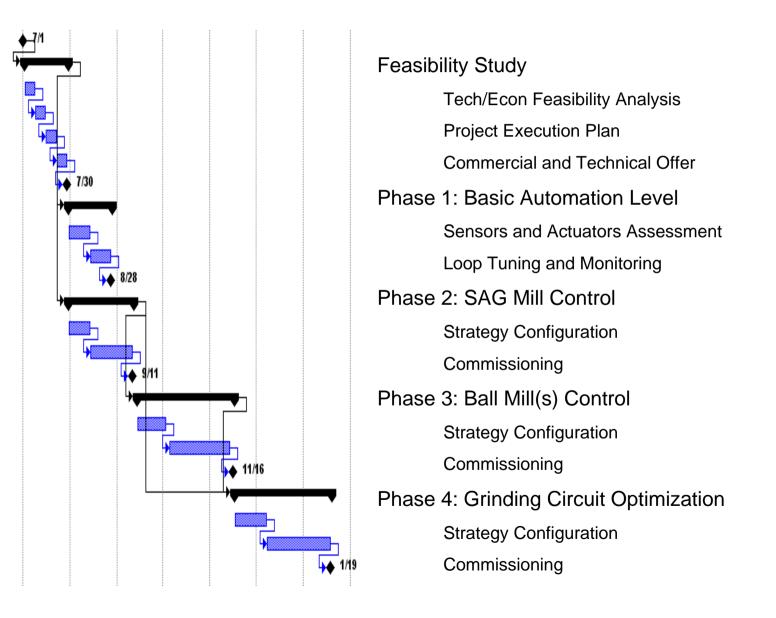


Grinding Plant Optimization

- Customer Value
 - Better grinding efficiency
 - Protect mill from ball impacts and thus mechanical damage
- Project Data
 - Execution in 3 phases
 - Base Loops
 - Individual Mill Stabilization
 - Coordination thereof via setpoint optimization
 - Total duration 6 months.
- Technology
 - Modular approach
 - Simultaneous and timely manipulation of
 - Ore Feed Rate
 - Mill Speed
 - Slurry Density
 - to achieve
 - Power and Bearing Pressure inside targets
 - Reduced quality variability

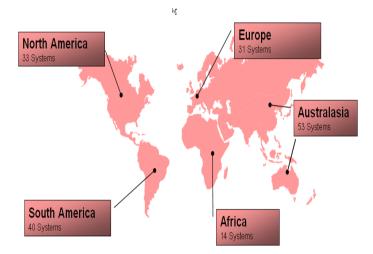


Grinding Plant Project Phases





Customer Value with cpmPlus Expert Optimizer







- Value we deliver to customer
 - Increased Output
 3% to 5%
 - Reduced Fuel Consumption
 3% to 5%
 - Reduced Emission Levels
 3% to 5%
 - Reduced Electricity Consumption 3% to 5%
 - Reduced Quality Variability
 10% to 20%
 - Reduced Refractory Consumption 10% to 20%
- Customers
 - Oil & Gas
 - Pulp & Paper
 - Minerals, Metals
 - Industrial Power



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